Updates from the Lab

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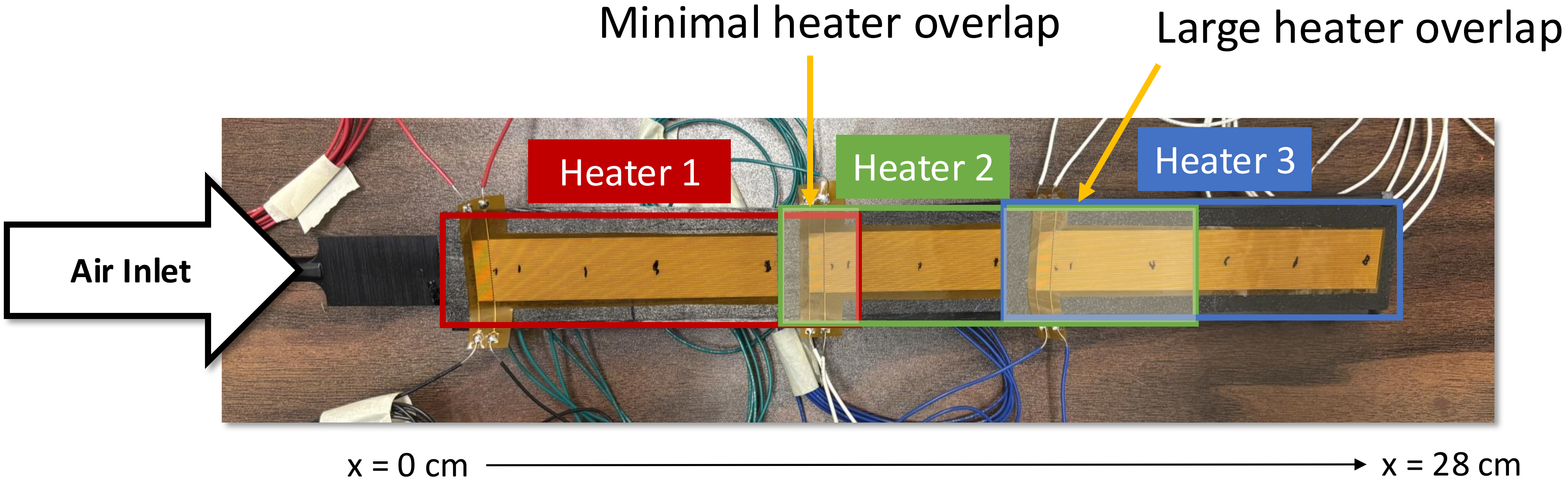
LBNL EIC meeting

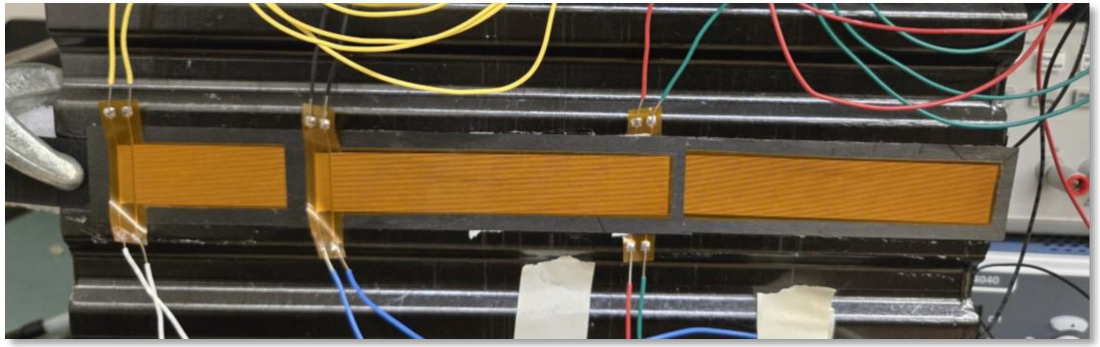
June 24, 2025

Testing Approach



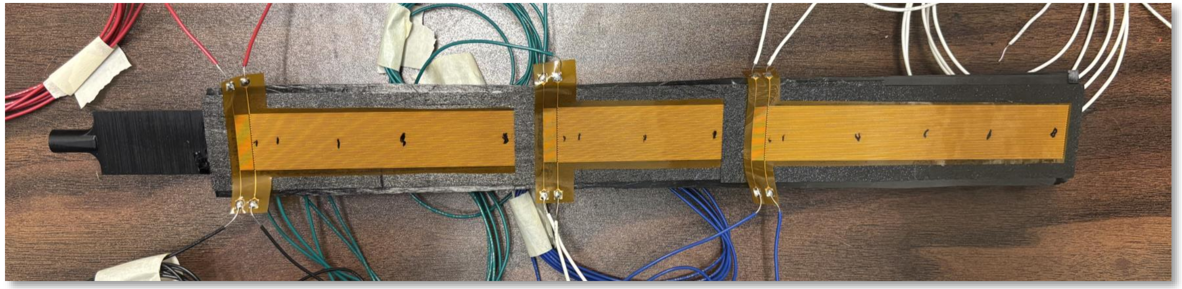
- Temp measured at different x values along corrugation (0 – 28 cm)
  - One point taken at each LEC position
- Data taken at 4-5 different air velocity values
- Taken at MAX and NOM powers

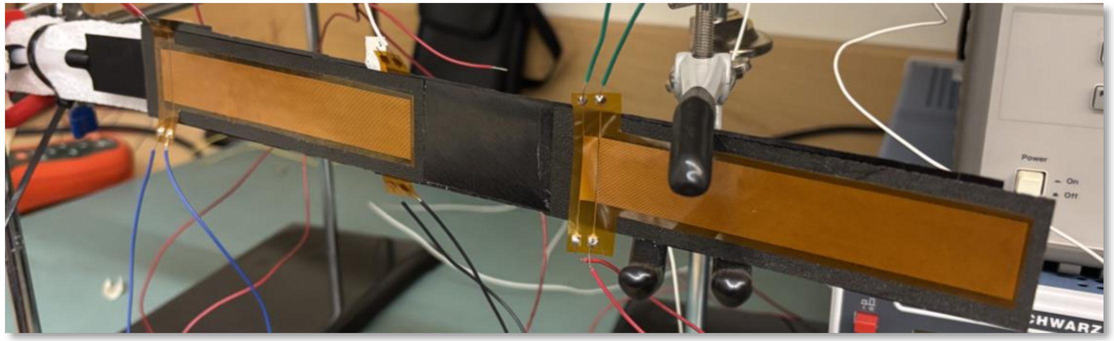
Thermal test pieces



Large corrugated piece with one channel used
All heaters outward facing
3rd LEC hidden

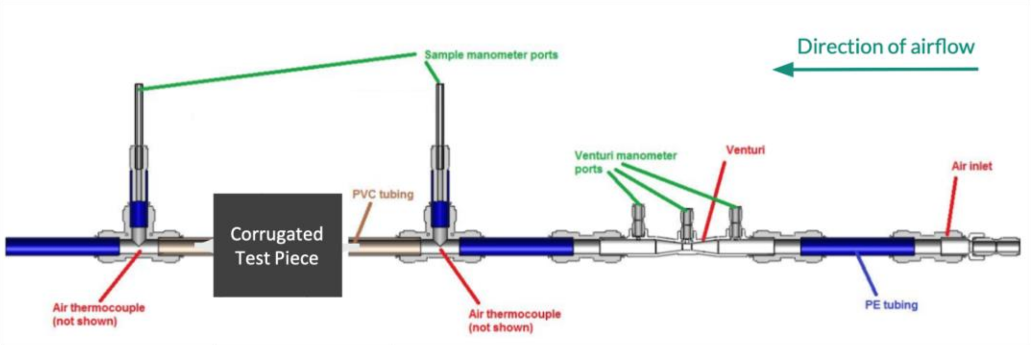
Single corrugation channel #1 & #2
All heaters facing outward
All LEC visible



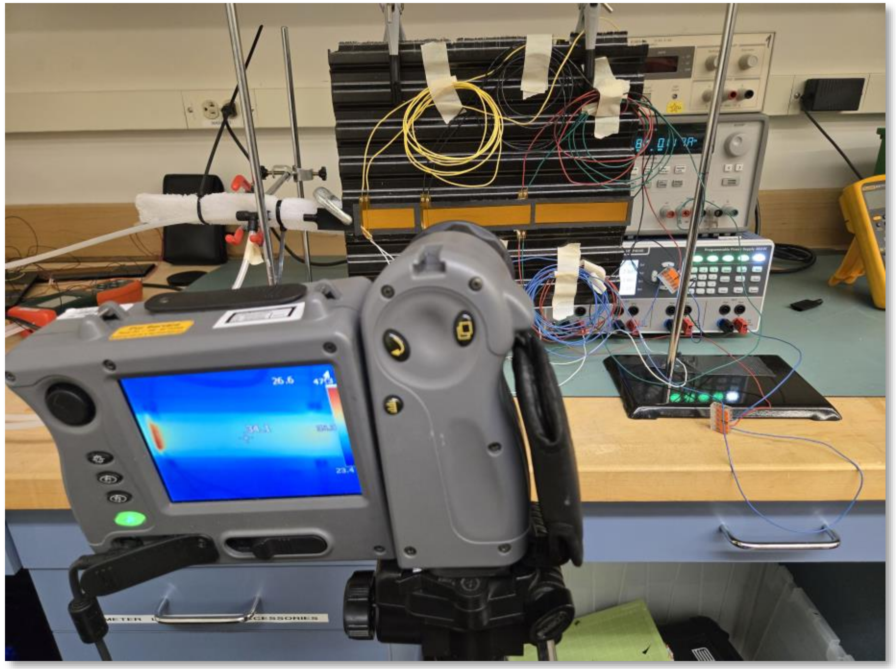


Single corrugation channel #3
One heater inward facing
2nd heater hidden

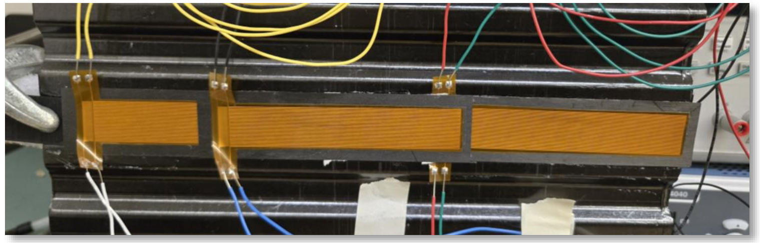
Test setup & caveats

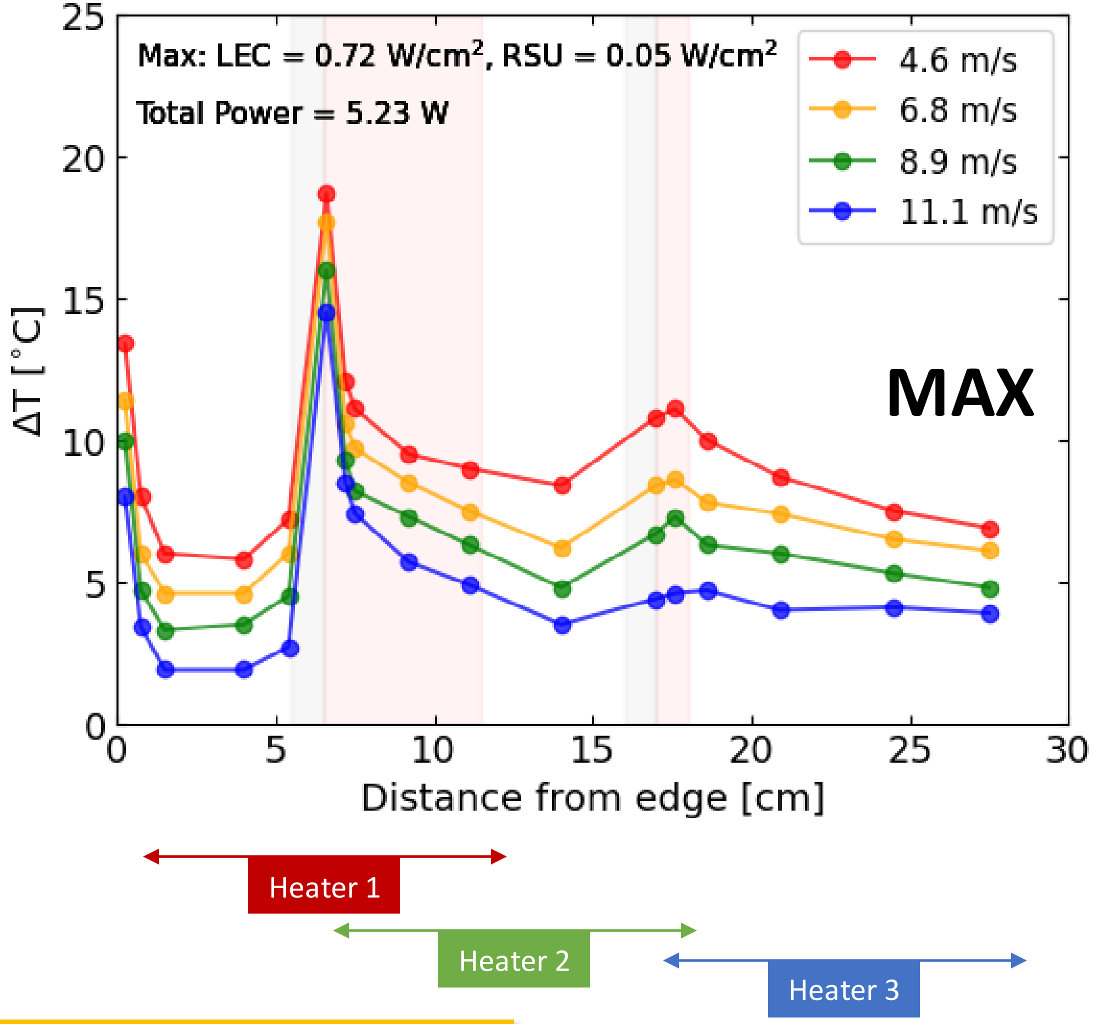


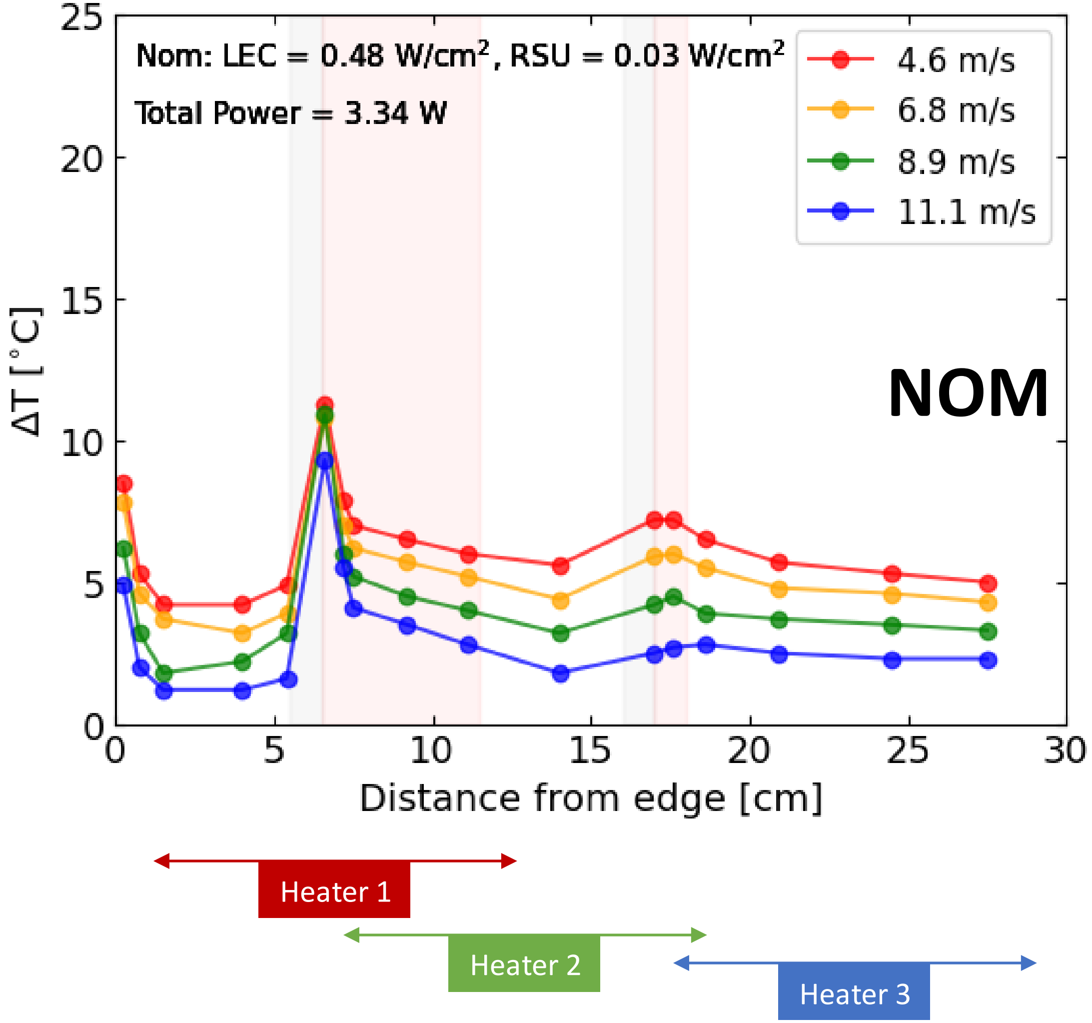
- Held in same orientation as planned in ePIC
- Using thermal camera → ~0.5°C fluctuations
- $\Delta T = T_{BrightTemp} - T_{DarkTemp}$
  - Dark temp taken with air flowing, but no power
  - Bright temp taken with air flowing and power on
- Cannot measure ΔT of sections we cannot see, i.e. hidden behind overlap
- Air velocity limited by setup safety



Large corrugated test piece



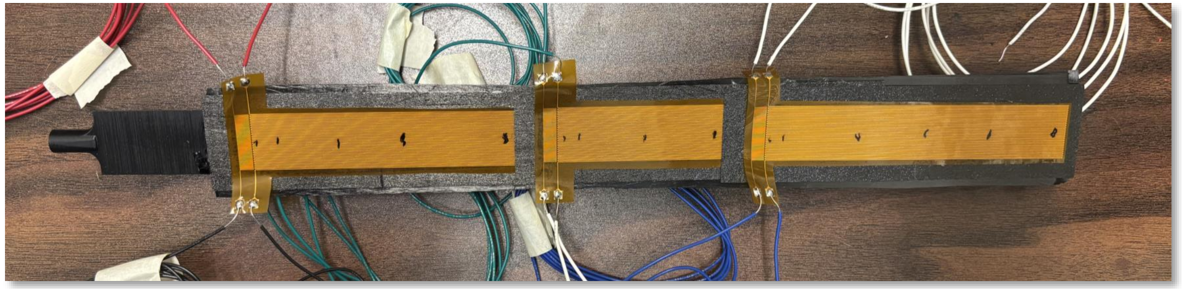


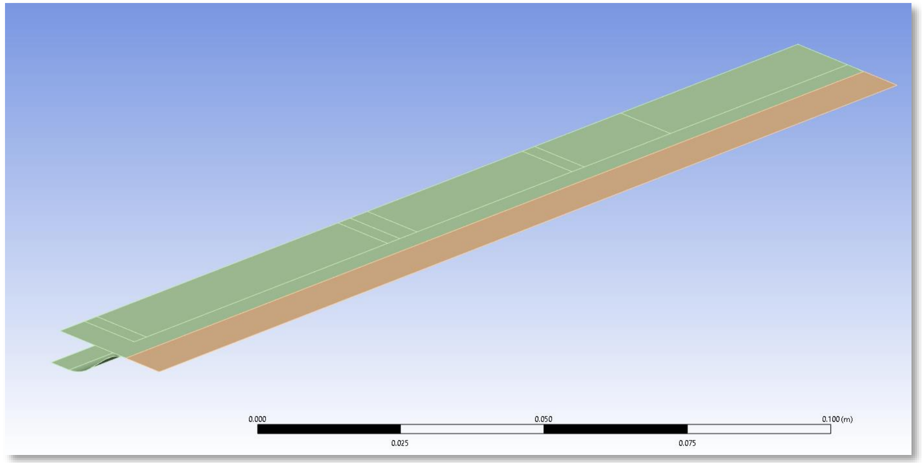


*LEC 3 cannot be directly measured

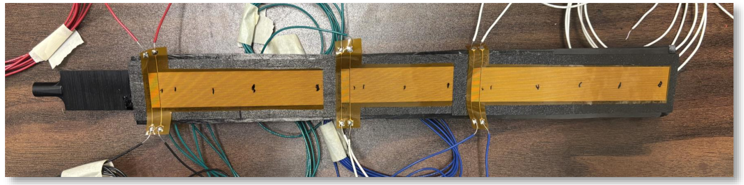
Single Corrugation Test Piece #1

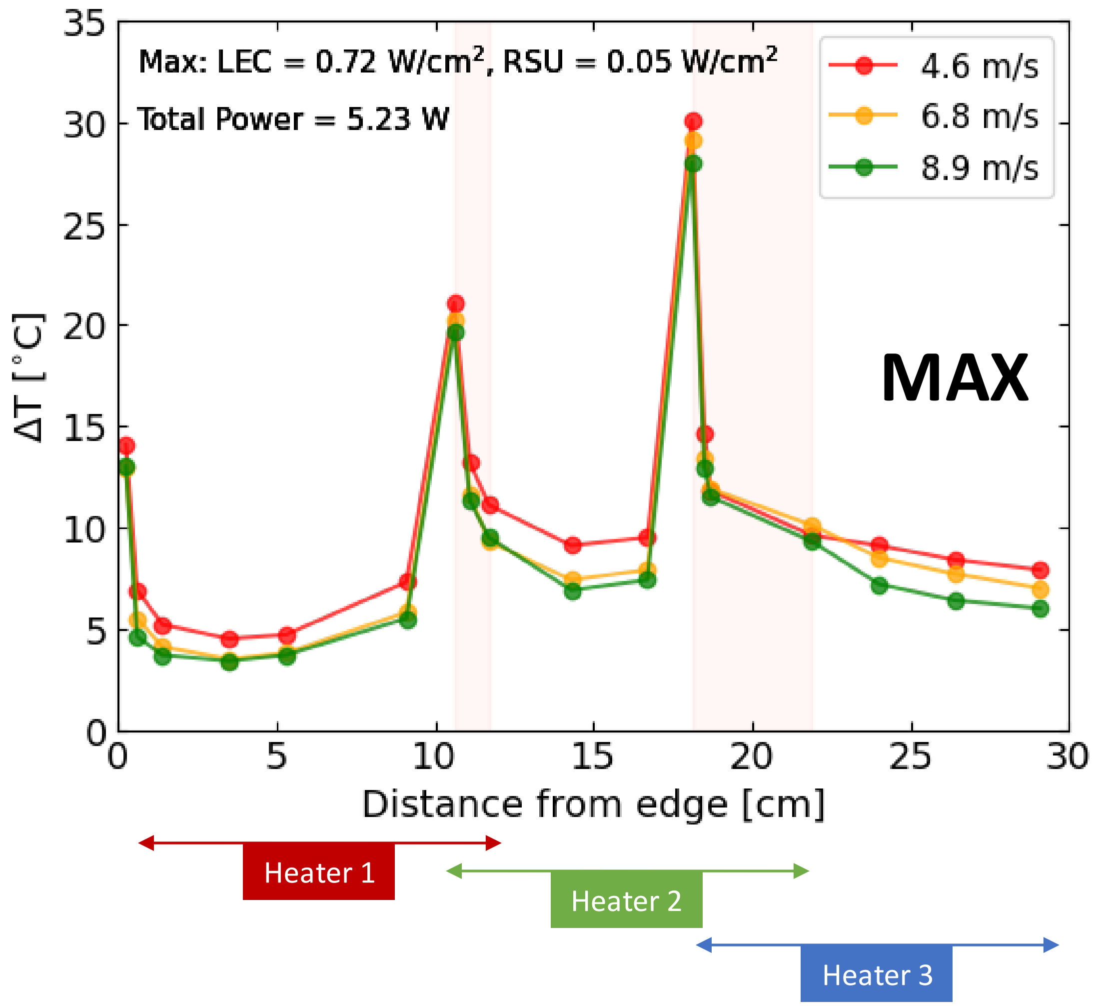
- Isolate natural convection & forced convection
- Minimize conduction through the corrugation
- Provide input to thermal model
- Expect T_{heater} to increase as T_{air} increases
  - T_{heater} should peak at the LECs (higher power density)

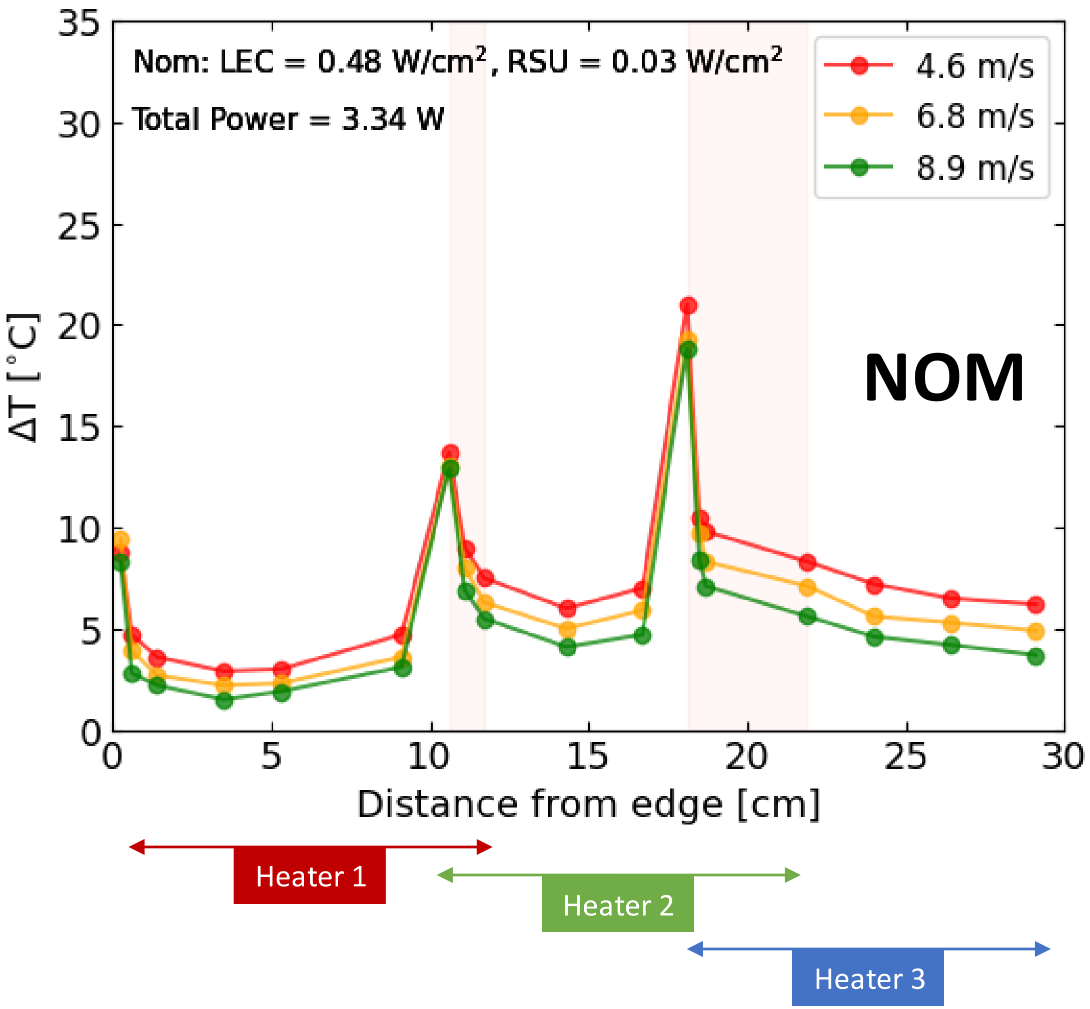




Thermal gradient



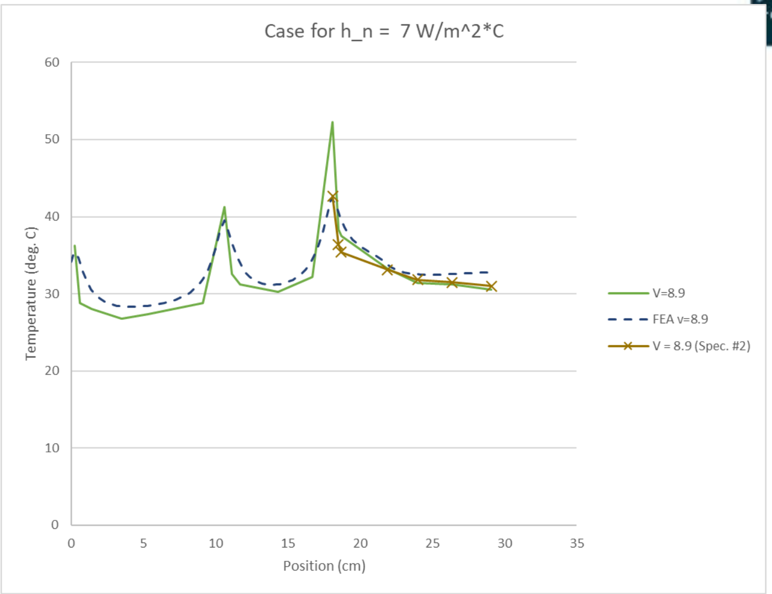


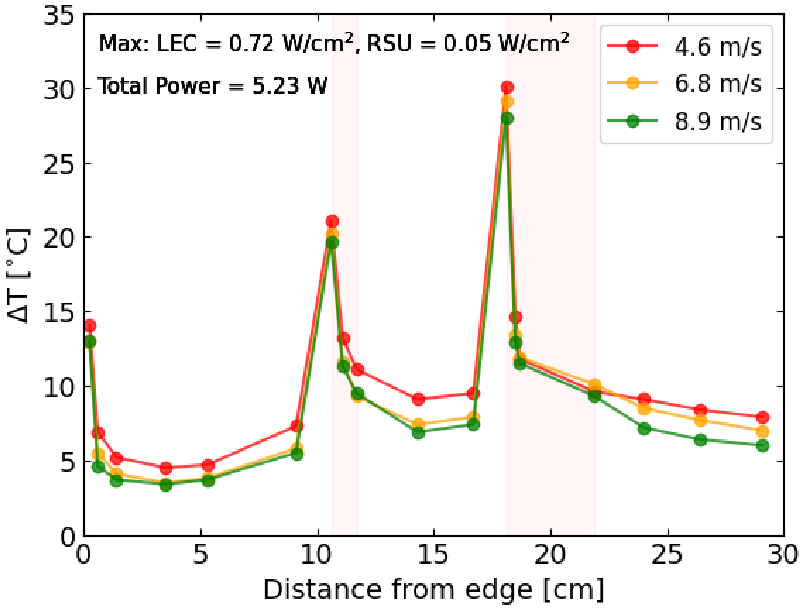


T does not vary much with air speed and significant T increase with each heater

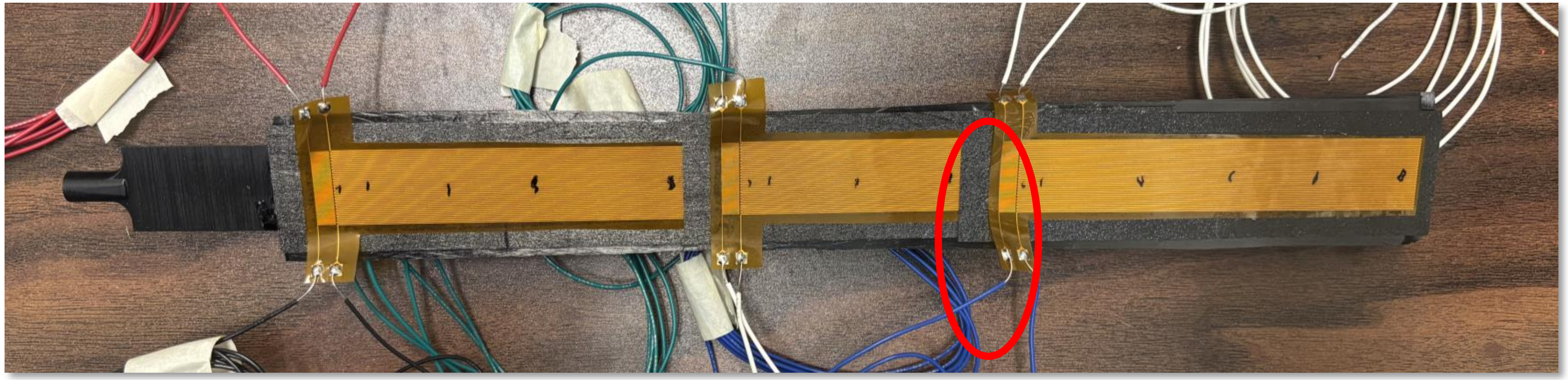
High ΔT investigation

- **Why is LEC 3 so much hotter than LEC 2?**
  - When individually powered, LEC 2 & 3 distributions should be the same. Both have overlap & are past the initial entrance zone region of the air flow
- Thermal model shows slight T increase per heater due to the increase in air temperature along the channel (1-2°C)
  - However, LEC 3 measures ~10°C greater than LEC 2
- **Why doesn't T vary with air speed?**
  - Previous results show ~1°C decrease per m/s increase
- Investigate this test piece and create a new one





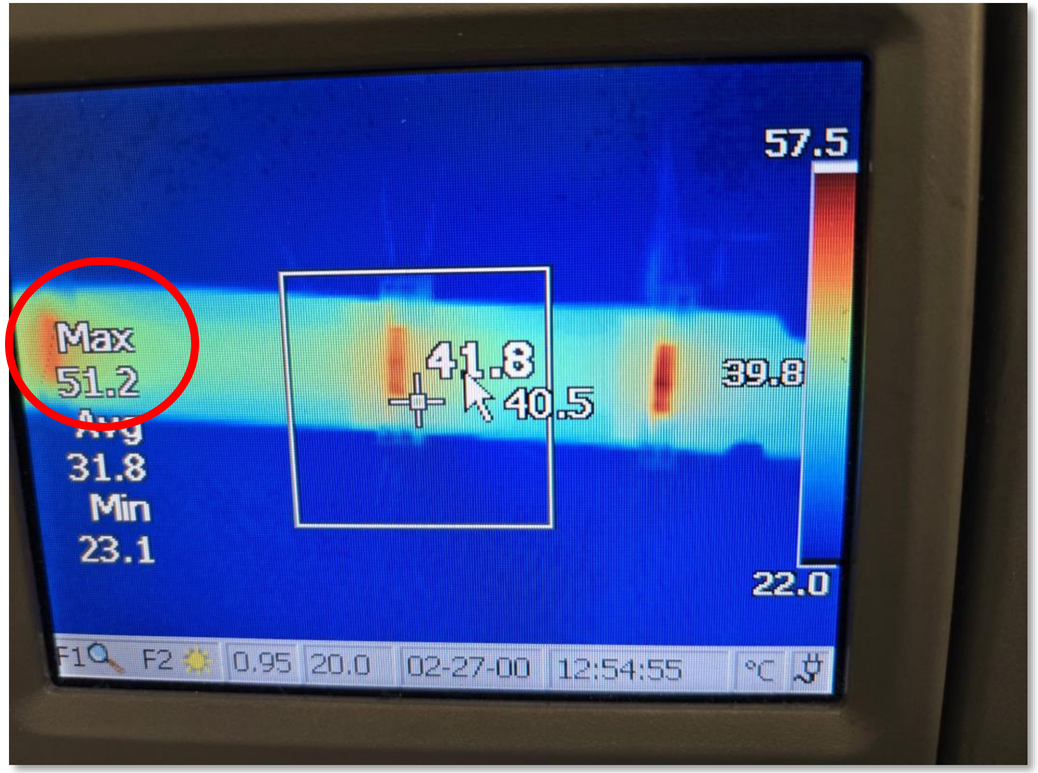
Heater adhesion



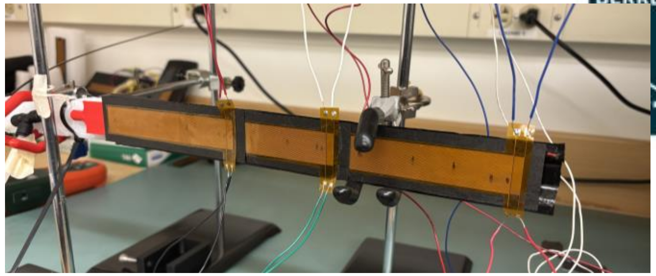
- Post inspection shows the delamination of the heater and larger than normal bonding material between layers was present.
- Without good adhesion, there is an air gap under the heater and the benefit of the CF conduction and the forced convection is lost.
- **Solution: Tighter control over adhesion procedure. Bonding under entire heater, not just copper traces**

Thermal camera: Max function

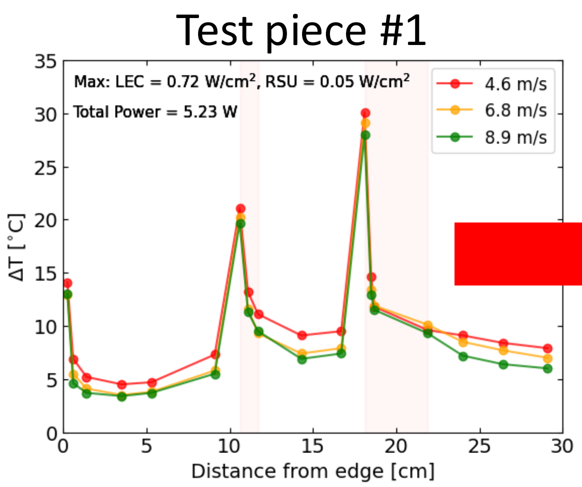
- Results shown used a different feature on the thermal camera: the **Max** function
- Will always find a hot spot and is not representative of the actual temperature
  - If hot spot is does not make contact with CF, it will never change with air velocity
- **Solution: Go back to taking average temperature along width of LEC**

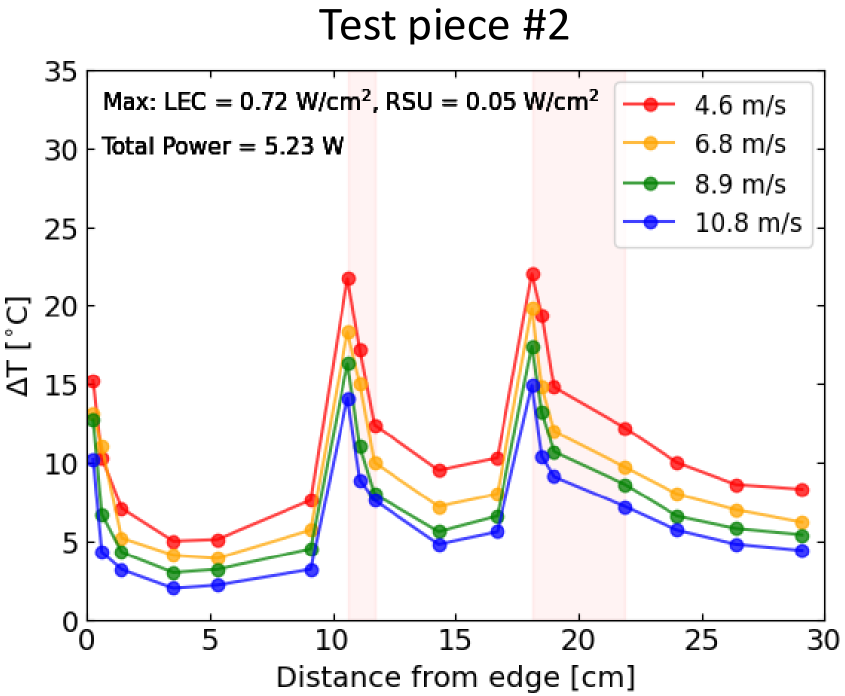


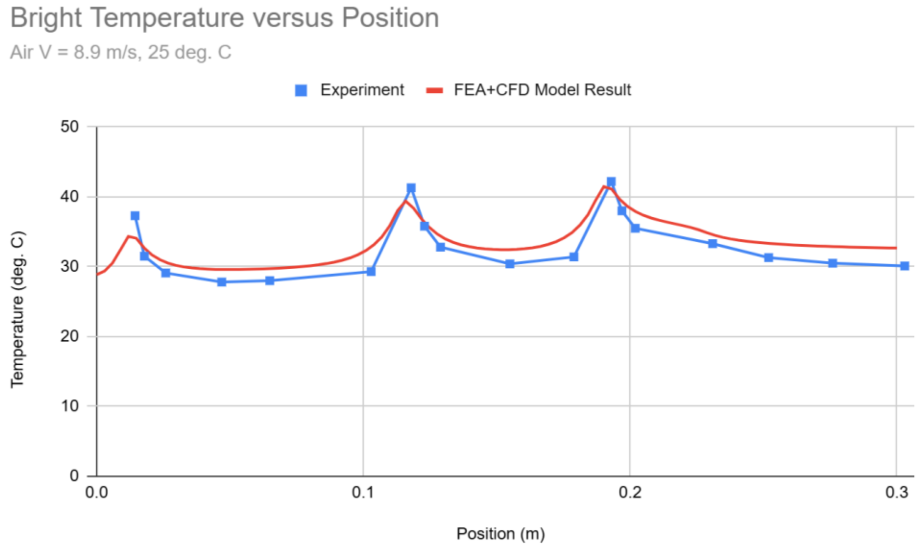
Single Corrugation Test Piece #2



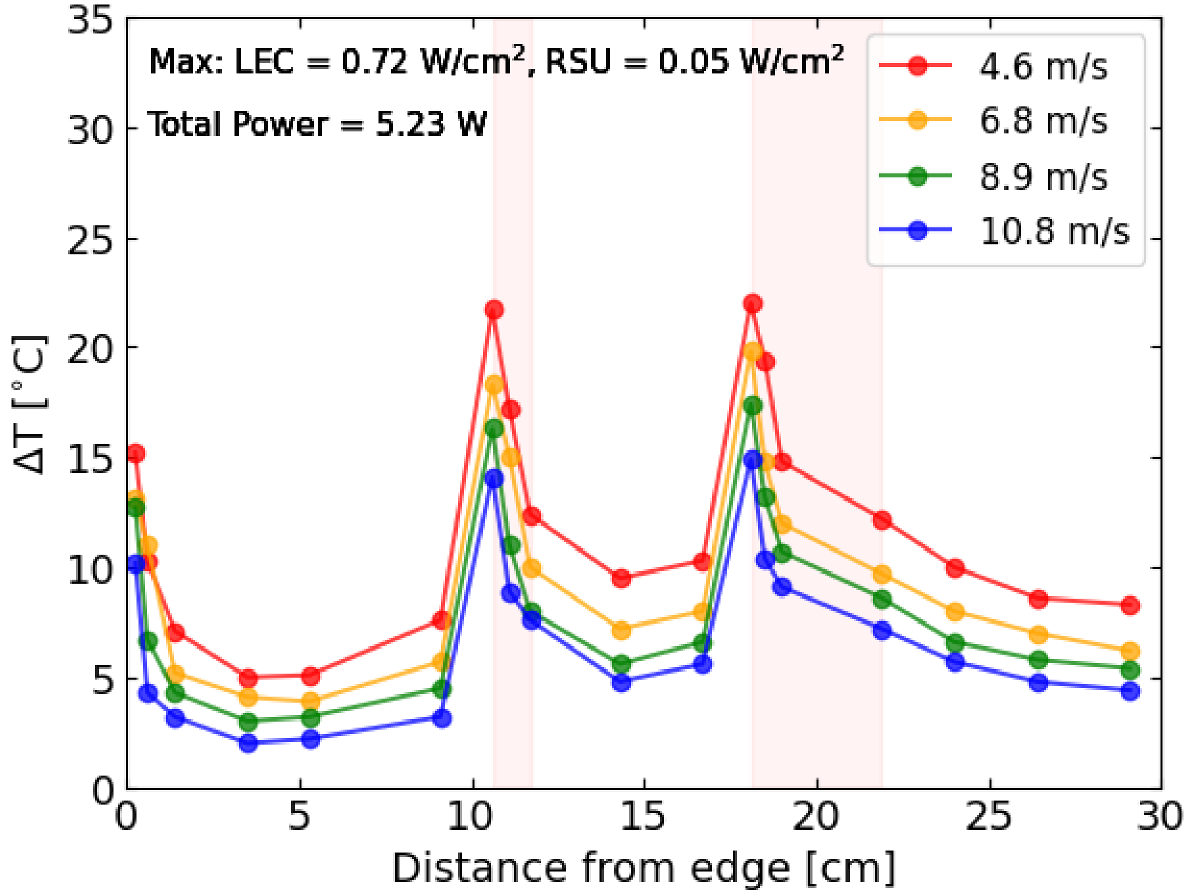
- Tighter control of bond thickness & adhesion under entire heater
- Measuring T directly (not Max function)
- Better agreement between LEC 2 & 3 and with model

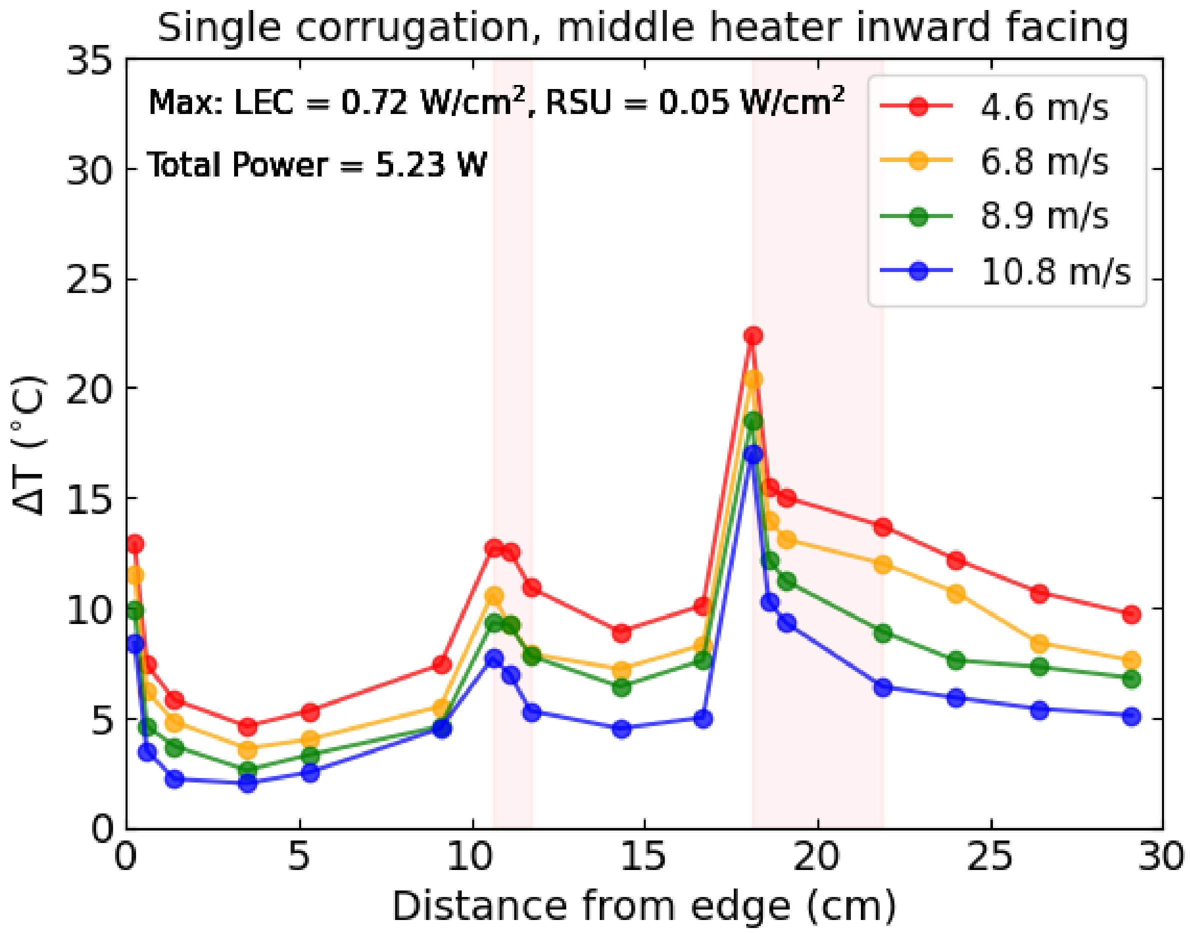






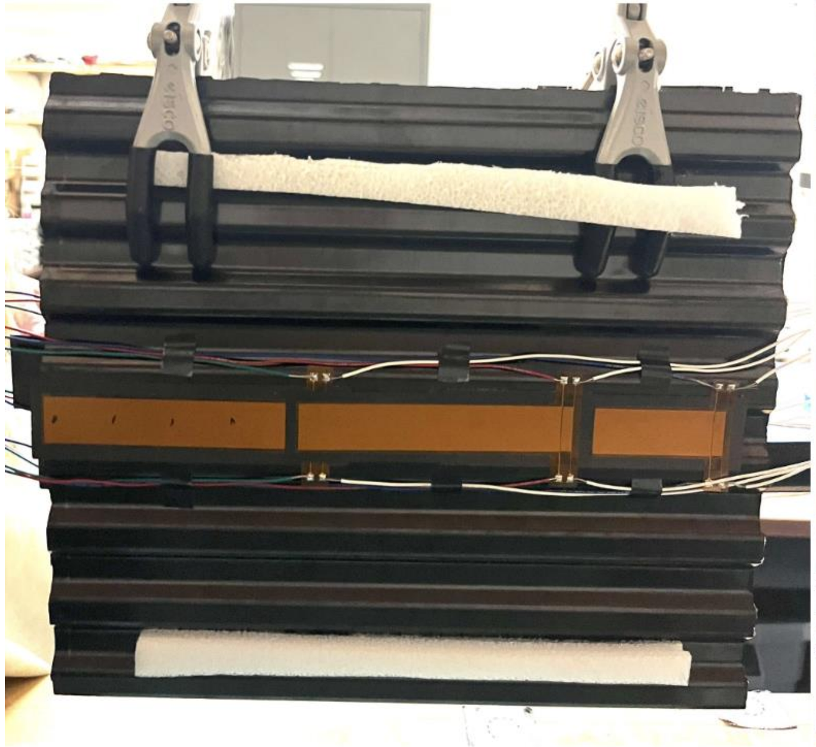
Comparison between #2 & #3

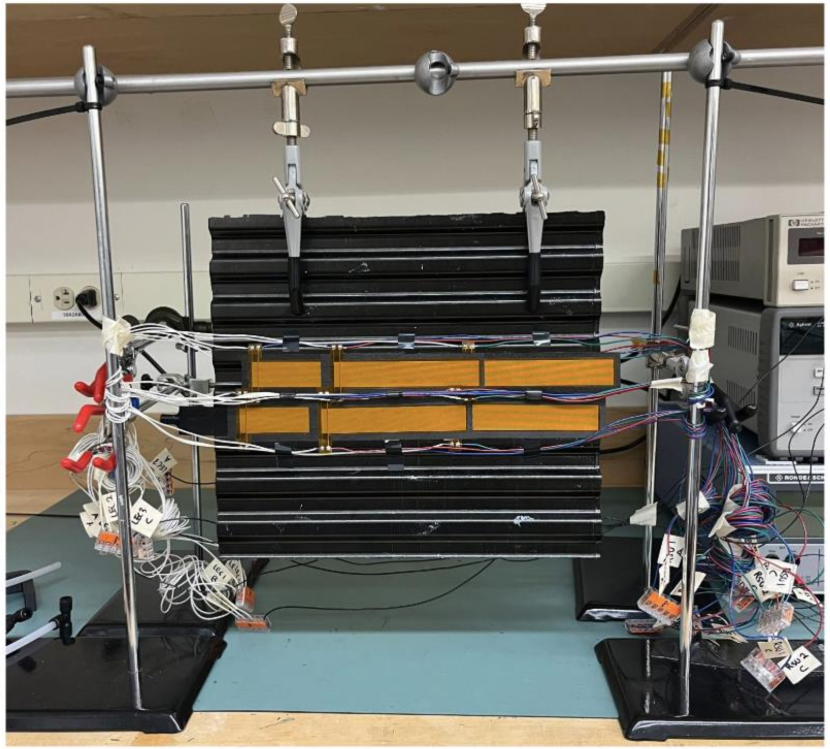




Upcoming

Credit: Katie Gray



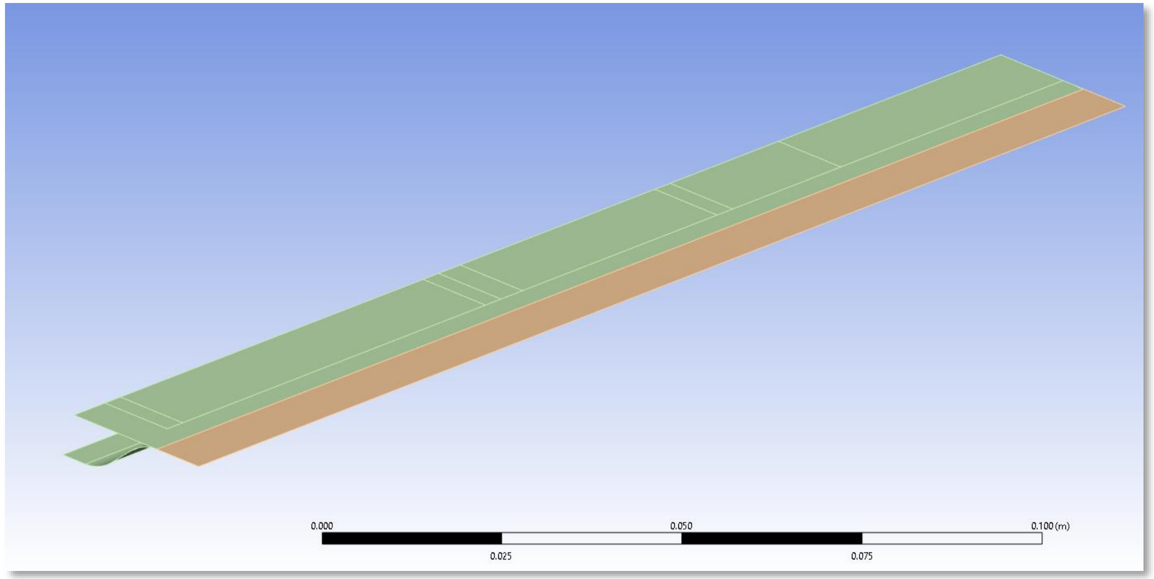


- In progress: Large thermal test piece with 3 channels filled
  - Test effects of proximity to neighbors

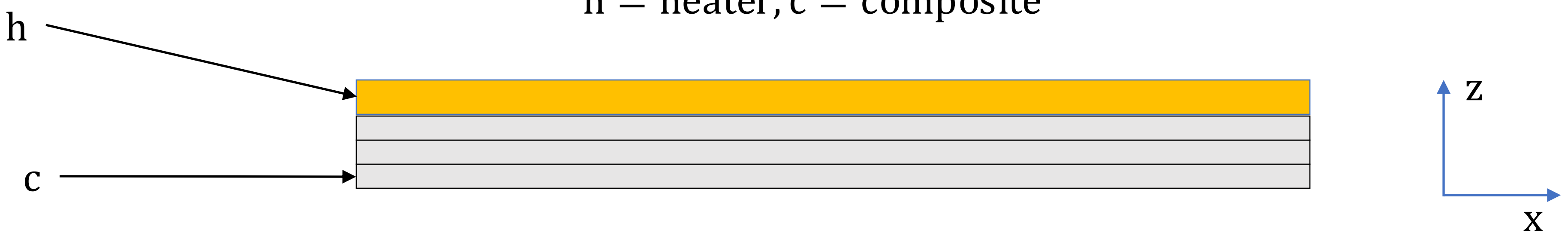
Backups

Modeling Approach

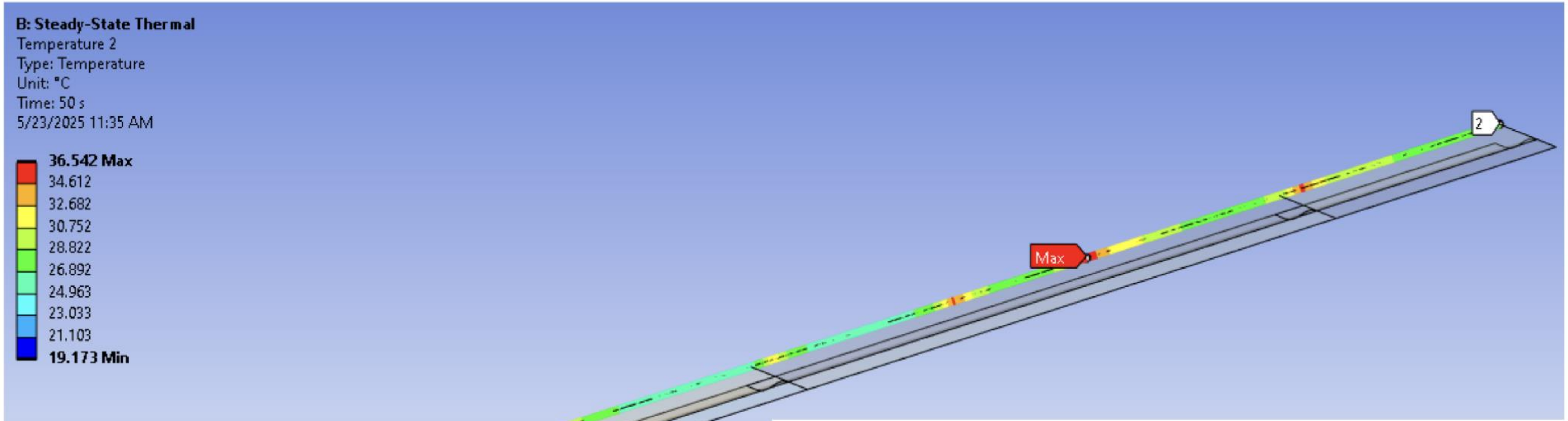
- Simplest model which captures thermal response.
- Shell model (2D) used instead of 3D components.
- Composite support and heaters homogenized into single part.

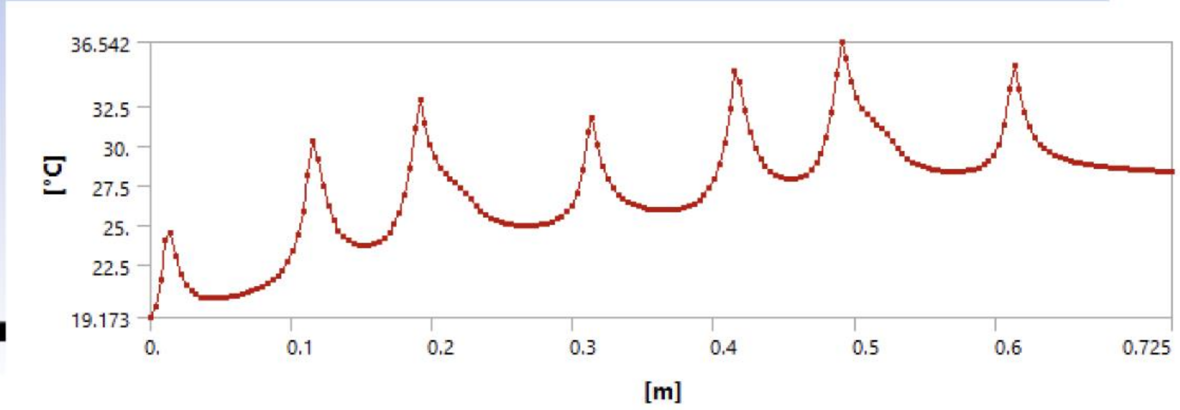


$$[0_h, 0_c, 90_c, 0_c];$$
$$\mathrm{h} = \mathrm{heater}, \mathrm{c} = \mathrm{composite}$$



Credit: Nick Payne





7 EIC-LAS in corrugation;
Temperature within req. range.

Forced Convection Model

- Using the Nusselt number to Gnielinski's correlation which is applicable to the transition flow region:

$$Nu_D = \frac{\left(f/8\right)(Re_D - 1000)Pr}{1 + 12.7\left(f/8\right)^{1/2}(Pr - 1)}$$

$$Re_D > 3000 \text{ and } Pr > 0.5$$

$$\boldsymbol{h_f = Nu_D \frac{\kappa}{D_H}}$$

For cooling air flow at 8.9m/s and initial temperature of 25°C (heating of air taken into account),

$$Nu_D = 15.9;\ h_f = 47.52\,\frac{W}{m{\cdot}K}$$

Entrance Region

- Nusselt number is inherently higher at the entrance of the duct.
- Analysis will use assumption that at inlet $Nu_D = 32$ and then scales to $Nu_D = 15.9$ at exit.
- Also temperature of air is at 25°C at inlet and scales to ≈30°C at outlet due to heating.